## **26** — Convective Transport [*Revision* : 1.3]

- Temperature Gradient
  - Recall from Notes 25:

$$\nabla = \left(\frac{\mathrm{d}\ln T}{\mathrm{d}\ln P}\right)$$

(a measure of temperature gradient);

$$\nabla_{\mathrm{ad}} = \left(\frac{\mathrm{d}\ln T}{\mathrm{d}\ln P}\right)_{\mathrm{ad}} = \frac{\gamma - 1}{\gamma}$$

(a measure of thermodynamic properties of gas);

$$\nabla_{\rm rad} = \frac{3\kappa\rho F}{4acT^4} H_P$$

(a measure of total flux).

- Condition for onset of convection:  $\nabla_{rad} > \nabla_{ad}$
- When convection sets in, how do we evaluate temperature gradient  $\nabla$ ?
- Split total flux into radiative and convective parts:

$$F = F_{\rm rad} + F_{\rm conv}$$

or

$$F_{\rm rad} = F - F_{\rm conv} = F\left(1 - \frac{F_{\rm conv}}{F}\right)$$

– Multiply both sides:

$$\frac{3\kappa\rho F_{\rm rad}}{4acT^4} H_P = \frac{3\kappa\rho F}{4acT^4} H_P \left(1 - \frac{F_{\rm conv}}{F}\right)$$

or

$$\nabla = \nabla_{\rm rad} \left( 1 - \frac{F_{\rm conv}}{F} \right)$$

- So, we can calculate  $\nabla$  from  $\nabla_{\rm rad}$  if we know what fraction of total flux is carried by convection
- **Observe**:  $\nabla \leq \nabla_{rad}$  from above, but  $\nabla \geq \nabla_{ad}$  for convection to continue.
- Convective flux
  - To date, no comprehensive, self-consistent theory for calculating  $F_{\rm conv}$
  - However, some progress can be made with mixing-length theory
  - Return to bubble from Notes 25. Assume bubble rises distance

$$\Delta r = \ell = \alpha H_F$$

before it dissolves into its surroundings;  $\ell$  is **mixing length**, usually representend in terms of dimensionless **mixing length parameter**  $\alpha$ 

- Heat released to surroundings, per unit volume, is

$$\delta q = C_P \rho \left( \Delta T^{(b)} - \Delta T^{(s)} \right)$$

where  $C_P$  is specific heat at constant pressure,  $\Delta T^{(b)}$  is change in temperature of blob (between start and end locations), and  $\Delta T^{(b)}$  is change in temperature of surroundings - For surroundings:

$$\frac{\Delta T^{(s)}}{T} = \left(\frac{\mathrm{d}\ln T}{\mathrm{d}\ln r}\right) \frac{\Delta r}{r} = \left(\frac{\mathrm{d}\ln T}{\mathrm{d}\ln P}\right) \frac{\mathrm{d}\ln P}{\mathrm{d}\ln r} \frac{\Delta r}{r} = -\nabla \frac{r}{H_P} \frac{\alpha H_P}{r} = \nabla \alpha$$

- For adibatic bubble motion:

$$\frac{\Delta T^{\rm (b)}}{T} = \left(\frac{\partial \ln T}{\partial \ln P}\right)_{\rm ad} \frac{\mathrm{d} \ln P}{\mathrm{d} \ln r} \frac{\Delta r}{r} = \nabla_{\rm ad} \, \alpha$$

- (note generalized definition of  $\nabla_{ad}!$ )
- So, heat released is

$$\delta q = C_P T \rho \left( \nabla - \nabla_{\mathrm{ad}} \right) \alpha$$

– If bubble moves with average velocity  $v_{\rm conv}$ , convective flux is

$$F_{\rm conv} = \delta q v_{\rm conv} = C_P T \rho \left( \nabla - \nabla_{\rm ad} \right) \alpha v_{\rm conv}$$

- ... which is desired result
- Convective velocity
  - What sets the velocity?
  - Recall: net force per unit volume on bubble is

$$f = g\left(\frac{\mathrm{d}\rho}{\mathrm{d}r} - \frac{1}{\gamma}\frac{\rho}{P}\frac{\mathrm{d}P}{\mathrm{d}r}\right)\Delta r$$

- After a bit of algebra:

$$f = g\rho \left(\nabla - \nabla_{\rm ad}\right) \frac{\Delta r}{H_P}$$

– Take average in moving from  $\Delta r = 0$  to  $\Delta r = \ell$  is

$$\langle f \rangle = g \rho (\nabla - \nabla_{\mathrm{ad}}) \frac{\alpha}{2}$$

– Work done per unit volume on bubble:

$$w = \langle f \rangle \ell = g \rho (\nabla - \nabla_{\mathrm{ad}}) \frac{\alpha^2}{H_P}$$

- Assume some fraction  $\beta$  of this work goes into bubble kinetic energy; so

$$\frac{\rho v_{\rm conv}^2}{2} = \beta g \rho (\nabla - \nabla_{\rm ad}) \alpha^2 H_P,$$

or

$$v_{\rm conv} = \left[2\beta g(\nabla - \nabla_{\rm ad})\alpha^2 H_P\right]^{1/2}$$

- Convection equations
  - Combine  $v_{\rm conv}$  expression with equation for convective flux:

$$F_{\rm conv} = C_P T \rho (\nabla - \nabla_{\rm ad})^{3/2} \alpha^2 \left(2\beta g H_P\right)^{1/2}$$

(Looks rather different to eqn. 10.100 of O&C, but should be essentially the same).

Also have

$$\nabla = \nabla_{\rm rad} \left( 1 - \frac{F_{\rm conv}}{F} \right)$$

- Two equations, two unknowns; solve for  $\nabla$  and  $F_{\rm conv}$
- Some Discussion
  - Suppose *all* flux is transported by convection; then, can calculate superadiabaticity:

$$\nabla - \nabla_{\rm ad} = \left[\frac{F}{C_P T \rho} \left(\frac{1}{2\beta g H_P}\right)^{1/2} \frac{1}{\alpha^2}\right]^{2/3}$$

- Deep in star, temperature and density large; temperature gradient close to adibatic ( $\nabla \approx \nabla_{ad}$ )
- In outer layers, temperature gradient quite superadiabatic; convection is inefficient because material cannot hold much heat
- Very close to surface, convective velocity becomes supersonic; signals breakdown of mixing length theory
- Also, in reality bubble motion is not adiabatic; must account for radiative losses to surrounding medium, and this complicates things somewhat